

Simulation of N₂/CH₄ Counter-Diffusion in Composite Membranes of the Type Silicalite-1- α -Alumina

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1. Introduction

The membrane model used describes (i) mass transport in macroporous support comprising diffusion in transition region between Knudsen and bulk diffusion superimposed on convective flow and (ii) mass transport in zeolitic phase accompanied by a parallel transport in defects of zeolitic layer. The mass transport in the support is described by Dusty Gas Model (DGM) and that in the zeolitic phase by Generalized Maxwell Stefan (GMS) approach. Parallel transport in defects of zeolitic layer is also described by DGM. Modelling is exemplified on dynamics of a semi-open Wicke-Kallenbach (W-K) cell (cf. Fig. 1) operated with a flat silicalite-1- α -Al₂O₃ membrane using a N₂/CH₄ mixture. It appeared that measurement of dynamic responses of the semi-open W-K cell represents a rapid method to characterize composite membrane quality.

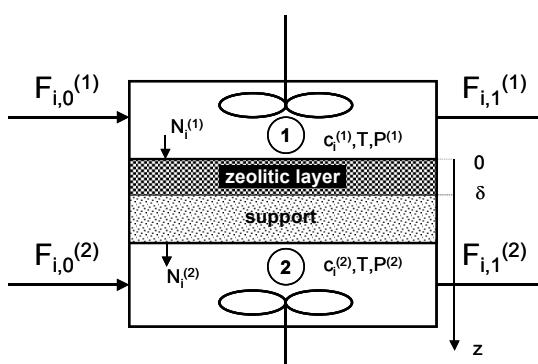


Fig. 1: Scheme of W-K cell

Semi-open W-K cell works with closed compartment (2). Dynamic responses of the cell evaluated with the system CH₄/N₂ are (i): $P^{(2)}_{\text{N}2}(\tau)$ and (ii) $P^{(2)}_{\text{CH}4}(\tau)$ i.e. single component responses to step change in $P^{(1)}$ at $\tau \rightarrow 0+$; (iii): $P^{(2)}(\tau) \equiv P_{\text{tot}} = P^{(2)}_{\text{N}2}(\tau) + P^{(2)}_{\text{CH}4}(\tau)$ started from the state $P^{(1)}_{\text{CH}4}(0) = P^{(2)}_{\text{CH}4}(0) = 0$ and $P^{(1)}_{\text{N}2}(0) = P^{(2)}_{\text{N}2}(0) = 100$ kPa by the step change to $P^{(1)}_{\text{N}2}(0+) = 80$ kPa, $P^{(1)}_{\text{CH}4}(0+) = 20$ kPa; (iv): $P^{(2)}_{\text{CH}4}(\tau)$ as the response to the same disturbance that defined in the case (iii).

2. Mathematical model

Mathematical model of the W-K cell which contains the above composite membrane involves the following relations:

- (i) Mass balance equations of mixture components in individual compartments
- (ii) Constitutive equations for components transport in silicalite-1 layer
- (iii) Mass balance equations of components in silicalite-1 layer

- (iv) Constitutive equations of components in defects of the silicalite-1 layer
- (v) Mass balance equations of components in the defects of the silicalite-1 layer
- (vi) Constitutive equations of components in the pore system of the support
- (vii) Mass balance equations of components in the pore system of the support
- (viii) Boundary conditions at silicalite-1 layer inlet and defect pore inlet
- (ix) Matching conditions at silicalite-1 layer - support layer interface
- (x) Boundary conditions at support outlet
- (xi) Matching conditions at the interface silicalite-1 matrix– defect pore

3. Examples of the simulation

Figure 2 shows the results of calculations as the normalized responses $X(\tau) = (P^{(2)}(\tau) - P^{(2)}(0)) / (P_{CH_4}^{(1)}(0+) - P_{CH_4}^{(1)}(0))$ of the total pressure in compartment (2) for a silicalite-1 membrane of the thickness 50 μm , free of the defects and with negligible mass transport resistance of the support. The total gas flow rate at the inlet of the compartment (1) i.e. $F_{N2,0}^{(1)} + F_{CH_4,0}^{(1)} = 360 \text{ ml}\cdot\text{min}^{-1}$.

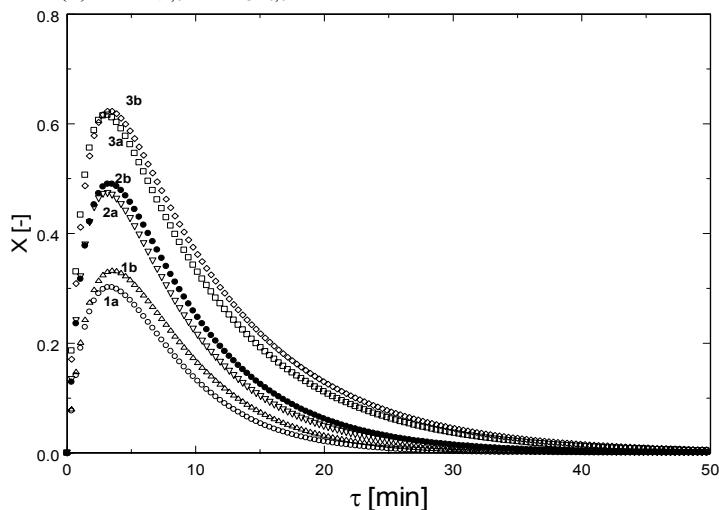


Fig. 2: Effect of Maxwell Stefan cross-diffusion coefficients D_{N2CH_4} on X vs. τ responses, Curves 1: $D_{N2} = 4.2 \times 10^{-9} \text{ m}^2\cdot\text{s}^{-1}$, $D_{CH_4} = 2.4 \times 10^{-9} \text{ m}^2\cdot\text{s}^{-1}$; Curves 2: $D_{N2} = D_{CH_4} = 3.3 \times 10^{-9} \text{ m}^2\cdot\text{s}^{-1}$; Curves 2: $D_{N2} = 2.4 \times 10^{-9} \text{ m}^2\cdot\text{s}^{-1}$, $D_{N2} = 4.2 \times 10^{-9} \text{ m}^2\cdot\text{s}^{-1}$; Curves a: effect of D_{N2CH_4} is disregarded; Curves b: effect of D_{N2CH_4} is considered

4. Conclusion

Simulator of dynamic responses in W-K cell for composite membranes of the type silicalite-1- α -alumina was elaborated as a tool to evaluate membrane defects.

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